

2011

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SUMMARY REPORT CC-88 INJECTION ON BOILER NO. 2 @ PT HIMALAYA TUNAS TEXINDO



PT MITRA CAHAYA MUKTI Rukan Puri Bintara Regency Blok S-3, JI Bintara Raya, Bekasi 17134 www.mitracm.com Asia Coal Catalyst Co: www.coalcatalyst.cor

Background

PT Himalaya Tunas Texindo has requested to increase their boiler efficiency on Energy. For over 6 months, PT Mitra CahayaMukti (M CM) as Asia Coal Catalyst Co's (ACCC) agent in country region and PT Himalaya Tunas Texindo (HTT) have been discussing to implement trial test for Coal Catalyst CC-88 at their plant. As a portion of this Trial Test it has been agreed that M CM & ACCC will demonstrate the combustion efficiency of its combustion catalyst CC-88 in a CFB boiler burning a common type of coal that HTT used daily.

This opportunity at HTT, located in Cisirung km.2, Moh Toha km 6.5, Bandung City, West Java Province, is an opportunity to demonstrate on Unit #2, a Circulating Fluidized Bed Boiler (CFB), recirculation boiler of an overall equivalent power rating of 5 Mwe and extract another 20 Ton per Hour of steam for their textile production. The coal comes from local Indonesia, probably Langkat Sumatera and having an average heat content of 5700 Kcal/kg gross caloric value, however we encountered coal having a heating range of 3572 Kcal/kg to 4325 Kcal/kg net caloric value and burns approximately 6.81 metric tons of coal per hour. Steam production is approximately 32 metric tons per hour (Ts/Tc=4.51) at the time of the demonstration.

Other information on this system is:

- No Lime stone injection for this boiler
- Recirculation of fly ash thru cyclone separator for re-burn
- Carbon content of collected fly ash approximately 7.61%
- Loss on Ignition approximately 8.89%
- There are 2 CFB boiler which is running in 2 x 100% scheme

Demonstration Concept

The demonstration concept was to determine how much less coal will be burned while injecting M CM & ACCC's combustion catalyst CC-88 under controlled conditions. The primary method to be applied is a total no of steam being produced with certain no of coal being burned before combustion catalyst CC-88 injected compared to nos of Ts/Tc being produce

after combustion catalyst CC-88 injected with some ratio , not taking into account of any boiler heat losses.

Simultaneously, M CM will be obtaining additional data from the Boiler Log Sheets as well as recorded data from the Boiler Control Modules. The purpose of M CM data gathering is determining information on Boiler Combustion Efficiency by the change in the Ts/Tc. This data will include:

- Boiler furnace temperatures
- Coal feed rate to boiler
- Steam production
- Emissions of particulate, O2
- Fly ash analysis and bottom ash analysis for carbon content
- Exit flue gas temperature

M CM provided all necessary data to HTT as well as HTT's staff recorded all daily log data as requested and oversaw the injection system operation. In addition, M CM provided the analysis of the emissions which available in HTT monitoring system, fly ash and bottom ash. In addition, M CM provided equipment to hold the Combustion Catalyst CC-88 as well as a measuring device to inject the CC-88 onto the coal screw feeder located on the 3rd floor of the Boiler House building. This equipment was a simple mini screw feeder to hold at least 10kg of CC-88. The injection is to have a 0.37kW motor at the side and having a mesh at top of hopper to prevent any large particles entering the throat area. In addition, an inverter will be installed at the control panel which was calibrated for the specific feed rates of 0.5 and 1.0 for the HTT Certified Test.

In addition, M CM provided sufficient amount of Combustion Catalyst CC-88 to conduct these tests delivered to the site in 11#-25 kg plastic pails.

Miscellaneous Items:

• Photographs were taken of the operations, PLEASE SEE APPENDIX

Goals

Each of the participating companies will have its individual goals of this demonstration.

• HTT: HTT would like to obtain how much reduction in coal can be achieved by the use of combustion catalyst CC-88 using the current coals. The results may allow them to reduce their operation cost. Other important information that may be important to the boiler operations are; quality of the new fly ash regarding the possibility of selling it for concrete aggregate, reductions in particulate emissions especially carbon carrying fine

particulate, and the chemical analysis of the new emissions Steam / Power Generation sizing capacity Study based on load list and equipment duty cycles and existing equipment data

• MCM & ACCC: M CM & ACCC are interested in obtaining information on the effectiveness of CC-88 when applied to coal combustion in Circulating Fluidized Bed Boilers (CFB) that have fly ash recirculation. This opportunity will provide us with data on improved combustion efficiency, emissions, fly ash analysis, the ability of improving the combustion characteristics of burning various quality coals, and overall boiler operating improvements

Executed Plan & Observations

The Proposed Plan involves five (3) Phases:

M CM developed and with the assistance HTT personnel, executed the actual testing in accordance with our Standard Test Procedures for Determining Combustion Efficiency for CFB Boilers.

<u>09/19 and 09/21/11 Installation Phase</u>. With helping of HTT's staff, M CM start installing the small injection device at 3 Nos of it's screw feeder each. The purpose to have this device is injecting at screw feeder according to 0.5kg/ton of coal ratio and 1kg/ton ratio by adjusting variable speed drive frequency at control panel to bring expected output of combustion catalyst CC-88. The program was set up a day to finish all , anyhow some changes to the operating procedure was extended for installing the device.

Observations:

- On Sept 21st M CM began to record the Base Line Data for 12 hours. The data was for Base Line, Phase #1.
- During this period, the #3 screw feeder feed rate & screw feeder totalizer are recorded.
- Our observation of the data looks very good. The Ts/Tc's are 4.51
- CC-88 started injection at 03:00AM on 09/22 entering phase 2
- Flys Ash & Bottom ash sample had been taken at end of phase 1

SEE APPENDIX FOR PHASE 1 RESULT

<u>09/22/11 Phase 2.</u> Immediately following Phase 1, CC-88 was injected at a rate of 0.5 kg/mt of coal at 03:00AM on 09/22 into the boiler along with the coal. After approximately 12 hours to

make boiler into equilibrium state the same procedure in Phase 1 was instituted. The results will be compared with Phase 1 result and a percentage improvement was determined.

SEE APPENDIX FOR PHASE 2 RESULT

Observations :

- On Sept 22nd 2011, 03:00PM data had been taken for phase1, the data was for phase 2 to be compare with phase 1, base line data
- Fly & Bottom Ash had been taken at the end of phase 2, significantly fly ash color had been changed much more whiter see appendix
- Fly ash lab result consist of 4.23% carbon content see appendix

<u>09/23/11</u> Phase 3. This phase 3 covers 1.0kg ratio of combustion catalyst CC-88 per ton of coal The data taken during this period seem to be correct as Ts/Tc actually went above the Base Line number and phase 2. At the time of this report, no issues had been found.

Observation :

- Data gathered from 03:00PM Sept 23th, 2011 and recorded after 12 hours of injection Combustion Catalyst CC-88
- Fly and Bottom ash had been taken at the end of phase 3

SEE APPENDIX FOR PHASE 3 RESULT

SEE APPENDIX FOR DATA SUMMARY

Review of Carbon Content of Fly & Bottom Ash and Observation

The analysis of the carbon content of the fly ash and bottom ash showed trending results. With the fly ash we would expect to have a reduction in the carbon content but not as significant as in the bottom ash. This is because the fly ash is re-circulated back to the furnace to obtain a second chance of burning the carbon and the bottom ash does not.

In all cases the fly ash content went as expected which we feel is in good result. the carbon content of the fly ash on 09/21 was higher than on 09/22. The Base Line Data for, no CC-88 injection. The carbon content of the fly ash was up 7.61% on 09/21 and having 44% reduction after injecting 0.5kg CC-88/ton and going down drastically to 67% during 1.0kg CC-88/ton.

In all cases that carbon content in fly ash show reduction after injecting CC-88 is supported by Loss on Ignition data.

SEE APPENDIX FOR FLY ASH RESULT

The Bottom Ash carbon content change was consistently down in all cases as would be expected. Down 43% the numbers given to us by the Institut Teknologi Bandung laboratory.

SEE APPENDIX FOR BOTTOM ASH RESULT

In reviewing the coal analysis, M CM feels that the stability in the coal chemistry most likely had the greatest impact on the performance as reported. In summary, See Appendix, as the days of the demonstration went on, the moisture content stable (showing correct improved efficiency), ash content quite stable, volatile matter stable providing proven heat available, to prove increasing combustion efficiency shown fairly.

Overview

- Consistent Data
- No equipment failure appear during test shown a good data
- Efficiency appeared to increase more when injection CC-88 at 1.0 vs. 0.5 kg/t coal. In the case of the CFBC boiler, it appears that an injection rate of 0.5 is having quite fast response for the operating condition and the dynamics of the furnace.

Conclusion

- Based upon the original ITB (Institute Technology Bandung), laboratory tests on the HTT fly ash produced during trials done in September 2011, it was probable that the full scale operations would produce an improved combustion efficiency (or reduced coal quantity). Our findings, showed an improvement of 4.91% at 0.5kg CC-88/ ton of Coal and resulting combustion improvement of 5.55% at 1.0kg CC-88/ton of coal.
- 2. Observations of the slagging within the boiler indicate that the CC-88 was beginning to remove the slag at the end of the demonstration cycle. If this is proven, the combustion efficiency and reduced coal consumption will improve further. Slag is an insulator and when it forms on the boiler tubes it reduces the rate of heat transfer from the hot furnace through the tube metal making steam inside the tubes.

- 3. O2 level increased with CC-88 injection which is opposite with expected value after using combustion catalyst, perhaps excess air is too high
- 4. The furnace temperature initially increased slightly with 0.5 injection but decreased from that with 1.0 injection. Reduction could be from lowering coal feed rate with 1.0 ratio. The exit flue gas temperature increased slightly indicating the coal feed could be reduced further.
- 5. There is a definite indication of the coal feed rate with 4.48% decreased at 0.5 and 9.29 at 1.0 injection, however the steam production dropped 0.72% at 0.5 and 2.69% at 1.0

SEE APPENDIX FOR A SUMMARY OF ALL DATA

Recommendation

- 1. M CM & ACCC recommends that HTT undertake a minimum six month long commercial operation of injection of an agreed level 0.5 kg/t of coal. During this period regular simple data gathering by the plant people can show certain trends. In addition, other trends can be determined on a cleaner boiler which will improve heat transfer to the steam, lower coal usage, lower emission levels (SO2, NOx, particulate), less carbon in fly ash and bottom ash, lower O2 levels, etc. over a long period. There is a possibility development of combustion efficiency while using this CC-88 over a long period to achieve boiler equilibrium state
- 2. Compare this six month test against an identical operating boiler, #1, Differences can then be measured that would provide side-by- side comparisons.
- 3. Following this six month operation, if successful
- 4. The Return on Investment (ROI) for HTT resulted in a 4.91% net coal cost savings, adding value to the plant's bottom line. The reduction of carbon and heat within the fly ash and bottom ash indicates an excellent reaction of the CC-88 catalyst with the coal in the furnace and provides backup to the percent improvements in combustion efficiency and reduction in coal demand. HTT may consider to produce more steam adding their production capacity in textile or having less coal to maintain same production as the time being.

Commercial

M CM has added commercial offer for HTT consideration including the illustration of cost saving per daily, monthly and annum basis.

PLEASE SEE APPENDIX













Fly Ash Sample at 1.0 CC-88 injection ratio

11 Nos of CC-88 pails for free trials

APPENDIX



PT. HIMALAYA TUNAS TEXINDO





-	9/21/2011												
			COAL FEED)	STEAM	COA	L SCREW ((RPM)	FURNACE TEMP.	EXHAUST GAS	0	2	NOTE
	HUUKS	SCREW 1	SCREW 2	SCREW 3	T/H	SCREW 1	SCREW 2	SCREW 3	°C	TEMP. (^o C)	1	2	NOTE
0	02.00 PM	686171	117819	445984									to get 12 hours
1	03.00 PM	686617	118260	446423	32.3	335	335	339	974	123	9.89	9.57	
2	04.00 PM	687034	118677	446841	31.7	370	375	378	952	120	8.62	8.7	
3	05.00 PM	687492	119120	447304	30.6	344	324	353	961	121	9.6	9.4	
4	06.00 PM	687954	119583	447771	34.7	345	347	351	977	120	9.51	9.19	
5	07.00 PM	688401	120032	448885	33.1	334	361	338	982	120	9.41	9.33	
6	08.00 PM	688859	120525	448691	33	357	361	369	966	119	9.09	8.83	
7	09.00 PM	689309	120976	449148	33.3	322	322	325	959	119	10	9.81	
8	10.00 PM	689707	121373	449548	30.9	345	347	349	953	119	9.86	9.18	
9	11.00 PM	690156	121823	450003	32.8	334	336	340	979	119	9.58	9.63	
10	12.00 PM	690625	122313	450480	34	333	398	340	968	120	9.42	8.36	
11	01.00 AM	691036	122749	450898	33.7	334	336	341	967	119	9.25	8.71	
12	02.00 AM	691480	123239	451348	36.6	334	336	337	956	121	10	9.56	
		5309	5420	5364	396.7	4087	4178	4160	11594	1440	114.23	110.27	Total
		29013.69	29620.3	29314.26	33.06	340.58	348.17	346.67	966.17	120.00	9.52	9.19	Avg. Base Line
		29.014	29.620	29.314			345.139					9.35	Avg. of two pts.
Total		87.948							973.17	120.83		9.46	Avg. 0.5 2 pts.
		7.33							969.00	122.08		9.68	Avg. 1.0 2 pts.
Average		8960150											



PT. HIMALAYA TUNAS TEXINDO



PT MITRA CAHAYAMUKTI





0.5 KG/T CC-88 INJECTION

_	9/22/2011												
			COAL FEED		STEAM	COA	AL SCREW ((RPM)	FURNACE TEMP.	EXHAUST GAS	C	2	NOTE
	HUUKS	SCREW 1	SCREW 2	SCREW 3	T/H	SCREW 1	SCREW 2	SCREW 3	°C	TEMP. (^o C)	1	2	NOTE
0	02.00 PM	696733	128451	456636									to get 12 hours
1	03.00 PM	697158	128875	457060	31.6	312	313	309	975	124	9.82	9.62	
2	04.00 PM	697574	129290	457475	34.4	323	325	325	963	121	9.74	9.51	
3	05.00 PM	697961	129682	457862	32.4	329	324	323	979	121	9.52	9	
4	06.00 PM	698416	130136	458317	32.8	357	361	367	998	121	8.81	8.274	
5	07.00 PM	698836	130557	458739	33.3	323	324	324	966	121	9.8	9.53	
6	08.00 PM	699258	130986	459161	34.8	322	323	323	973	121	10	9.43	
7	09.00 PM	699678	131406	459581	33.9	333	335	338	971	121	9.56	9.1	
8	10.00 PM	700089	131818	459992	32.4	321	321	320	974	121	8.89	9.78	
9	11.00 PM	700558	132287	460457	31.2	321	322	324	974	120	9.91	9.62	
10	12.00 PM	701024	132753	460922	32.4	321	335	338	971	120	10	9.44	
11	01.00 AM	701413	133150	461317	32.3	320	373	336	968	120	9.34	9.26	
12	02.00 AM	701782	133560	461690	31.9	333	339	337	966	119	9.64	9.37	
		<u>5049</u>	5109	5054	393.4	3915	3995	3964	11678	1450	115.03	111.934	Total
		27592.79	27920.685	27620.11	32.78	326.25	332.92	330.33	973.17	120.83	9.59	9.33	Average
		27.59279	27.920685	27.62011			329.83					9.46	Avg. of two pts.
Total		83.13358			393.4								
		6.93											
Average		9095529											

TS/TC = 4.732 4.732 Combustion Efficiency Result :

4.911% 4.911%

PT. HIMALAYA TUNAS TEXINDO



PT MITRA CAHAYAMUKTI





1.0 KG/T CC-88 INJECTION

	9/23/2011												
			COAL FEED)	STEAM	COA	AL SCREW ((RPM)	FURNACE TEMP.	EXHAUST GAS	C	2	ΝΟΤΓ
	HOURS	SCREW 1	SCREW 2	SCREW 3	T/H	SCREW 1	SCREW 2	SCREW 3	°C	TEMP. (⁰ C)	1	2	NOTE
0	02.00 PM	706937	138795	466880									to get 12 hours
1	03.00 PM	707373	139229	467324	36.2	323	324	327	981	124	9.41	9.15	
2	04.00 PM	707799	139654	467752	31.5	313	311	311	957	124	9.89	9.4	
3	05.00 PM	708202	140055	468154	34.9	312	311	313	982	125	9.85	9.38	
4	06.00 PM	708642	140493	468598	30.3	324	324	326	985	123	9.11	8.78	
5	07.00 PM	709033	140930	468987	32.7	310	308	312	976	122	9.61	9.48	
6	08.00 PM	709501	141393	469452	30.3	311	309	310	970	121	9.84	9.36	
7	09.00 PM	709865	141754	469814	33.5	309	308	307	965	121	10.1	9.52	
8	10.00 PM	710246	142133	470194	32.3	319	320	323	975	122	10	9.49	
9	11.00 PM	710682	142565	470629	32.4	310	305	310	970	121	10.5	9.84	
10	12.00 PM	711081	142959	471026	32.2	310	305	310	969	122	10.4	9.69	
11	01.00 AM	711479	143351	471417	32.4	310	306	309	955	120	9.9	9.51	
12	02.00 AM	711923	143834	471874	32.1	296	331	304	943	120	10.2	9.91	
		<mark>4986</mark>	5039	4994	390.8	3747	3762	3762	11628	1465	118.81	113.51	Total
		27248.49	27538.135	27292.21	32.57	312.25	313.5	313.5	969.00	122.08	9.90	9.46	Average
		27.24849	27.538135	27.29221			313.08					9.68	Avg. of two pts.
Total		82.07884			390.8								
		6.840											
Avera	ige	9227749											

TS/TC = 4.761 4.761

Combustion Efficiency Result :

5.557% 5.557%



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Laboratorium Buangan Padat dan B3 Labtek IX C Lantai 4 Telp/Fax : 462 22 2534187

HASIL ANALISA LABORATORIUM Lab. Result of Analysis

Limbah/Wasie Tanggal /Date Sumber/Source Analisa/Tested Pemesan/Principa/ *

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PT. Himalaya Tunas Texindo C- Organik PT Mitra Cahaya Mukti

22 September 2011

No.	Kode Sampel	Satian	Hasil Analisa
FÓR	MA		
1.	Fly ash	% BK	7,61
2.	Bottom Ash	% BK	5,43
FOR	MB	5.	-
3.	Fly ash	% BK	4,23
4.	Bottom As	% BK	3,06
FOR	M C		
5.	Fly ash	% BK	2,49
6,	Bottom Ash	% BK	5,40*)

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Sheep in strength

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Cat : BK = Berat Kering

*) possible sample fix up or not correct

Bandung, 5 Oktober 2011 Kepala Lab./Head of Laboratory,

BLAB. SOL ID AND HAZARADUS WASTE

Dr.\Env. Eng. Sukandar NIP\132 316 903

My Doc/Data Lab. 2011/Masil Analisa Lab.

Laboratorium Buangan Padat dan B3

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Up BR Brog. Stayam

HASIL ANALISA LABORATORIUM Lab. Result of Analysis

Limbah/Waste Tanggal /Date Sumber/Source Analisa/Tested PemesaniPrincipal

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Fly ash (FORM A) 22 September 2011 PT. Himalaya Tunas Texindo 1 Oksida - Logam : PT Mitra Cahaya Muktl

No.	Parameter	Satuan	Hasil Analisa
1.	SiO ₂	% BK	64,89
2.	Fe ₂ O ₃	% BK	10,56
3.	Al ₂ O ₃	% BK	6,66
4.	K ₂ O	% BK	0,17
5.	Na ₂ O	% BK	0,19
6.	CaO	% BK	4,78
7.	mgQ	% BK	3,76
8.	TiÔ2	% BK	0,09
9.	P2O5	% BK	0,11
10.	LOI	% BK	8,89
11,	SO3	% BK	0,001

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 $\frac{1}{2} \sum_{i=1}^{n} \frac{1}{2} \sum_{i=1}^{n-1} \frac{1}{2} \sum_{i=1}^{n-1}$

Cat : BK = Berat Kering

Bandung, 5 Oktober 2011 Kepala Lab./Head of Laboratory,

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NIP. 132 316 903

My Doc/Data Lab. 2011/Ilasil Analisa Lab.

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> Analisa/Tested Pemesan/Principal

HASIL ANALISA LABORATORIUM Lab. Result of Analysis

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Fly ash (FORM B)
25 September 2011
PT. Himalaya Tunas Texindo
Oksida - Logam
PT Mitra Cahaya Mukti

No.	Parameter	Satuan	Hasil Analisa
1.	SiO ₂	% BK	72,01
2.	Al ₂ O ₃	% BK	11,45
3.	Fe ₂ O ₃	% BK	6,85
4.	K₂O	% BK	0,11
5.	Na ₂ O	% BK	0,15
6.	CaO	<u>%</u> BK	5,17
7.	MgQ	% BK	3,02
8.	TiÔ ₂	% BK	0,15
9.	P ₂ O ₅	% BK	0,08
10.	LOI	% BK	1,22
11.	SO3	% BK	0,001

Cat : BK = Berat Kering

Bandung, 5 Oktober 2011 Kepala Lab./Head of Laboratory,

LAB SOLID AND HAZAR Dept. Environmental en MM /1 M Dr. Env. Eng. Sukandar NIP. 182,316 903

My Doc/Data Lab. 2011/Hasil Analisa Lab.

Laboratorium Buangan Padat dan 83





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HASIL ANALISA LABORATORIUM

Lab. Result of Analysis

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Limbah/Waste Tanggal /Date Sumber/Source Analisa/Tested Pemesan/Principal

Fly ash (FORM C) 25 September 2011 PT. Himalaya Tunas Texindo Oksida - Logam PT Mitra Cahaya Mukti

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No.	Parameter	Satuan	Hasil Analisa
1.	SiO₂	% BK	65,23
2.	Al ₂ O ₃	% BK	11,11
3.	Fe ₂ O ₃	% BK	7,24
4,	K₂O	% BK	0,18
5.	Na ₂ O	% BK	0,19
6.	CaÓ	% BK	5,11
7.	MgO	% BK	3,33
8.	TiQ ₂	% BK	0,11
9.	P2Ô5	% BK	0,07
10.	LOI	% BK	6,66
11.	SO3	% BK	0,001

Cat : BK = Berat Kering

Bandung, 5 Oktober 2011 Kepala Lab./Head of Laboratory,

LAB. SOLIO AND HYZARODUS WAST NUNIN Dr. Env. Eng. Sukandar

NIP. 182 316 903

My Doc/Data Lab. 2011/Hasil Analisa Lab.

Laboratorium Buangan Padat dan B3

FORM A

14.00	686171	117 819	445 384	33.0	347	360	333	958	112	9.30	START
Real forder and social second second	l .	COAL FEED	and the second	FLOW	(OAL SCREW (RP	M)	FURNACE TEMP.	EXHAUST GAS	O2	
Н	SCREW 1	SCREW 2	SCREW 3	T/H	SCREW 1	SCREW 2	SCREW 3	IIC	TEMP. (IC)	VALUE	
15 100	686 617	118260	446 422	32-3	335	335	339	974	123	9.89 9.57	
16 200	687034	118677	446 841	31,7	370	375	378	352	1.30	8.62 8.70	1
17.300	687092	119120	1447304	30,6	344	329	333	9613000	13:131	19.6019.40	120
18 400	687444	119 583	da 777	347	345	1337	1351_	977-	120	19.519.19	
19500	688401	120032	448225		339	361	-338-	<u> </u>	120	3.41 3.53	
20600	688859	120525	448691		357	361	369	966	119	3.09 0.09	<u> </u>
8		1								<u> </u>	
9											
10											
11											and the second
12	-										All the state of the
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24					and the second s				<u></u>	+	
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FORM A

		COAL FEED		FLOW	C	OAL SCREW (RPI	A)	FURNACE TEMP.	EXHAUST GAS	O2		N
Н	SCREW 1	SCREW 2	SCREW 3	T/H	SCREW 1	SCREW 2	SCREW 3	UC	TEMP. (IC)	VAL	UE	
1	JORENT	COTTON IN				a Construction of the Cons				10.0	9-81	
1					an and the full second s		Contract of the second s	v		````		
	<u>gx</u>				and a substantial second s							AND THE OWNER WATER OF THE STREET
3	1 az					A CONTRACTOR OF	and the second se					an fa tha ann an a
4 E	10-1											
0	BORNA SORMA											
0	10 QA 2 Adt	170071	4140	222	372	322	325	959	119	10.00	9.81	
21. /	609200	101202	644840		340	347	349	953.	113	9.86	9.18	
22 0	689101	121313	474000	29.8	224	336	340	979	119	9.58	9.63	
23 9	690136	12 0 2 1 0	450480	30.0	332	398	340	968	120	9.42	8.36	
29 10	1040625	100 740	A 50 908	23 1	334	336	341	967	119	9.25	8.71	
0111	691030	126 149	1-1210	36 6	238	336	337	956	121	10.0	9.56	BOTTOM AS
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24											<u> </u>	
Total	1										<u> </u>	
	TOFP D.										Louisenences	
Average												



FORM B



u			COAL FEED		FLOW	C	OAL SCREW (RPA	A)	FURNACE TEMP.	EXHAUST GAS	O2	
1	SC	REW 1	SCREW 2	SCREW 3	T/H	SCREW 1	SCREW 2	SCREW 3	D OC	TEMP. (0C)	VALUE	
31	691	960	123761	451835	34.0	321	3021	321	983	121	9.80 9.38	
4 2	697	1363	12A183	452241	29.8	332	329	333	934	118 1	10.2 9.48	***** *******************************
53	69	2792	124603	452677	34.7	332	331	337	976	113	10.0 9-64	
6 4	693	237	125039	453128	34.2	395	407	399	950	120	10.1 9.48	
25	693	\$674	125485	953571	32.0	345	345	351	969	119	9.62 9.28	
6	694	f104	125904	454002	31.5	344	348	351	948	120	9.72 9.53	
<u>65</u> 7		<u>+·</u>										
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9	4	Same	<u></u>		an and the state of the	and an ever a supply of the product of the second second second second second second second second second secon		- Prove Participation and a second				
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13	-	1 a			and the second discourse of the second discourse of the second discourse of the second discourse of the second					1		and and the contract of the second
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15												and a state of the
10								lan tanàn dia 12 mangana dia 10 m dia mandritra dia mandritra dia mandritra dia mandritra dia mandritra dia man N				
9 0010	10.0	600	12 - 201	100.	1 - 0			1999				
QU 10	699	8-20	150986	459/61	24.8	32.2	323	323	973	121	10.0 9.43	
- 18	1979	618	131406	A50 501	19 35.5		335	<u> </u>	271	121	9.56 9.10	
20	1900	089	131810	45-9992	32.4.	321	381	320	974	121	9.89 9.78	www.communication
21	100	SSR	132287	460457	31.2	331	322	324	974	120	9.91 9.62	
22	101	024	132753	760922	32.9	321	225	338	971	120	10:0 9.44	
· 23	10	1413	138100	461317	32.3	520	373	336	968	120	9.34 9.26	
Total	10	1182	133.560	461690	51.9	3.3.3	23.0	337	266	119.	9.60 9.87	
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FORM B

H	COAL FEED			FLOW	COAL SCREW (RPM)			FURNACE TEMP.	EXHAUST GAS	O2	ey penyi kang bang bang panya kang bang bang bang bang bang bang bang b
	SCREW 1	SCREW 2	SCREW 3	T/H	SCREW 1	SCREW 2	SCREW 3	.)C	TEMP. (0C)	VALUE	1
1			and the second			CANADA AND A CANADA					
2									1		
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6							and the second				
7	1694 175	125 975	454073	33.7-	346	386	338	962	120°C	18.6 11.4	M2: 26,0
8	KAGGOS	126 240	454 506	322	347	349	357	959	112	9.47 9.28	MER :
9	695000	126 Zgi	454914	32 6	346	350	359	583	115	9.49 9.25	-MI, MZ
10	695449	127233	455359	22 a	335	336	339	api	122	3.86 8.66	MLOFF
11	695878	122626	455785	22.2	323	356	314	<u> </u>	124	11.1 11.1	MI. W5.1
12	696299	128034	456196	31.41	324	328	340	528	1jag	9,14 0.82	
13	196723	128 451	456636	33.3	225	3.57	325	955	1-124	9.50 9.42	- Th
14	1697 150	128 875	957060	31.6	372	313	309	<u> 395</u>	124	4.89 962	A Transformerense
15	697574	129290	457475	54.4	323	325	325	6.63	1291	3.74 9.51	
16	697961	129682	457862	32.4	329	329	323	9.75	121	9.52 9.00	atar n
17	698416	130136	458 317	32.8	357	361	367	396	121	8-81 8-2	H BBLO
18	69.836	130557	- 4+0736	333	323	324	324	966	121	9.00 9.5	MI, MZ,
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Total				á feir a start	[<u> </u>	
	1									-	
Average							L	L		L	

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FORM C



COAL FEED			FLOW	COAL SCREW (RPM)			FURNACE TEMP.	EXHAUST GAS	O2		
SCREW 1	SCREW 2	SCREW 3	т/н	SCREW 1	SCREW 2	SCREW 3	°c	TEMP. (°C)	VAI	LUE	
702285	134079	462108	32.4	3212	323	322	956	119	10.2	9.43	
702615	139 909	462 528	32.7	329	323	3, 2.3	955	120'	10.5	9.80	
703058	134842	A62 983	31.5	321	321	32.2	967	110	10.2	9.95	
703494	135229	463 370	32.3	321	\$20	322	946	120	10.8	10.1	
703896	135683	463824	53.5	366	370	375	968	122	8.85	8.61	
704323	136118	464255	33.3	331	334	33.6	946	122	10.2	9.78	
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			a na an								
2-2-00-2	1. 24-	11 0 9 10	3	9 14	dh d	P / An	0.7/2	121	9 84	0 21	Participant and a second s
109501	141593	469452	<u>50 · 4</u>	211	227	210	Ar m	121	10.0	9.52	And the state of the second system of the second system of the second system of the second system of the second
109865	141754	769819	22.3	2019	300	1 207	JUES DOE	141	10.0	9.20	
10.140	142.133	410194	36133	319	300		020	124	10.5	a.R.	
10006	142.565	47000	58.9	2112	305	110	040	12.7	10 3	G 60	
11081	147.959	47/020	36.V	310	106	1 210	aren	12.02	0.90	In CI	
T1 440	199751	APA 871.	30 11	200	3.341	3.01	NG 3	120	10.2	0.47	
1 1969	1999030	-191 590	<u>y.</u> p., Q	and a second	1	1			1		
			na internet statement of a submitting a submitting and a submitting a submitting a submitting and a submitting						1		and the second
			an a		ana managena ang kanang ka	20 Carlon Carlon Contraction (Carlon Contraction Contraction)		sart) - and the second framework and the second			
	SCREW 1 7022.85 70264 703058 703494 703896 704323 704323 704323 704323 709865 710245 710245 710245 710245 710245 710245 711682 711682	COAL FEED SCREW 1 SCREW 2 702285 134079 702645 134079 703058 134843 703058 134843 703058 134843 703058 135229 703896 135683 704323 136118 704323 136118 709865 141393 709865 141754 710245 142959 71081 142959 71181 142959 71184 142844	$\begin{array}{c c c c c c c c c c c c c c c c c c c $	$\begin{array}{ c c c c c c c c c c c c c c c c c c c$	$\begin{array}{c c c c c c c c c c c c c c c c c c c $	$\begin{array}{ c c c c c c c c c c c c c c c c c c c$	$\begin{array}{ c c c c c c c c c c c c c c c c c c c$	$\begin{array}{ c c c c c c c c c c c c c c c c c c c$	$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$	$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$	$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$

FORM C



Н	COAL FEED			FLOW	COAL SCREW (RPM)			FURNACE TEMP.	EXHAUST GAS	O2	
	SCREW 1	SCREW 2	SCREW 3	T/H	SCREW 1	SCREW 2	SCREW 3	D ₀ C	TEMP. (°C)	VALUE	
1	1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 - 1997 -										
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3		1							1		1
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6											
7	704406	136 197	4643 41	34.3	321	156	321	934	122	12.0 11.0	1 (n)
8	704718	136 562	469717	32.2	334	335	340	961	123	10.919.4	3
9	705220	137056	965 169	32.0	321	323	337	a76	129	10497	8
10	705 698	132476	465599	35.0	346	351	354	9:05	124	9.5 9.2	6
11	\$06007	137932	466038	21.4	323	326	323	977	120	9.99 3.5	2
12	706539	1383 79	966990	220	305	325	325	1006	124	10.4 10,0	9
13	706937	130795	96600	32.0	313	312	315	306	124.	9.87 9.5	3
14	707373	139229	467324	36,2	323	324	327	901	129	9419.1	2
15	707799	139659	467752	315	313	311	311	957	120	9.89 9.4	6
<u>p 16</u>	708262	140055	468 154	34.9	312	311	313	982	25	9.85 9.3	2
17	1708642	140493	468590	30.3	329	329	326	9.25	165	9.118.7	8
18	709033	190930	468987	32,7	310	308	312	976	122	9.9.9.9	8
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